# Survey of Catalysts for Oxidation of Mercury in Flue Gas

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DOE/NETL Mercury Control Technology Conference Pittsburgh, PA December 2006





## **Mercury in Flue Gas**

- Elemental mercury (Hg<sup>0</sup>)
  - Emitted from high-temperature coal combustion
  - Insoluble in water
  - Can be removed with activated carbon injection (ACI)
- Oxidized mercury (Hg<sup>2+</sup>)
  - Typically assume HgCl<sub>2</sub>
  - Water soluble, sorbs to AC
- Particle-bound mercury (Hg(p))
  - Both Hg<sup>0</sup> and Hg<sup>2+</sup>
  - Typically a small fraction of total mercury
- Ratio of Hg<sup>0</sup>/Hg<sup>2+</sup> depends on a number of factors (coal-Cl, LOI, time-temperature history, etc.)



# **Mercury Removal Technologies**

#### Activated carbon injection (ACI)

- Inefficient mixing/contact: Requires C/Hg mass ratios>1000:1
- AC is a general sorbent
- Potentially makes fly ash unusable as cement additive
- Low cost: AC costs < \$1/lb</p>
- Current 'best bet'

#### Catalytic mercury oxidation

- Use catalyst to convert Hg<sup>0</sup> to Hg<sup>2+</sup>
- Removal of Hg<sup>2+</sup> with wet FGD (>90% efficient)
- Proposed catalysts: SCR catalysts, carbon-based materials, metals and metal oxides

There is no "magic bullet" – mercury control will involve multiple technologies/products

#### Major Uncertainty: Reaction Mechanism

- Assumption: Chlorine (HCl or Cl<sub>2</sub>) is the oxidizer for mercury in flue gas
- Hg<sup>0</sup>(g) + HCl(g)/Cl<sub>2</sub>(g) is too slow to explain observed extents of oxidation
  - -Hg<sup>0</sup>(g) + Cl(g) is fast, but Cl(g) concentrations are low
  - Cl<sub>2</sub> could be catalytically generated from HCI (Deacon process), but Cl<sub>2</sub> concentrations are generally low
- Likely oxidation mechanism is heterogeneous



## **Heterogeneous Reaction Mechanisms**

Langmuir-Hinshelwood

$$A(g) \leftrightarrow A(ads)$$
 $B(g) \leftrightarrow B(ads)$ 
 $A(ads) + B(ads) \xrightarrow{k_{surf}} AB(ads)$ 
 $AB(ads) \rightarrow AB(g)$ 

- Reaction between adsorbed Hg<sup>0</sup> and HCI
  - Both Hg<sup>0</sup> and HCl can adsorb to carbon sorbents



## **Heterogeneous Reaction Mechanisms**

#### Eley-Rideal

- Reaction between an adsorbed species and a gasphase species
- -Either Hg<sup>0</sup> or HCl can be the adsorbed species

$$A(g) \leftrightarrow A(ads)$$

$$A(ads) + B(g) \xrightarrow{k} AB(g)$$



## **Heterogeneous Reaction Mechanisms**

#### Mars-Maessen

- Hg<sup>0</sup> reacts with lattice oxidant (O or Cl)
- Oxidant is replenished from gas-phase

$$A(g) \leftrightarrow A(ads)$$

$$A(ads) + M_x O_y \rightarrow AO(ads) + M_x O_{y-1}$$

$$M_x O_{y-1} + \frac{1}{2}O_2 \rightarrow M_x O_y$$

$$AO(ads) \rightarrow AO(g)$$

- This mechanism may explain effectiveness of halogenated sorbents
  - Lattice halide could serve as the oxidant



## **Other Major Questions**

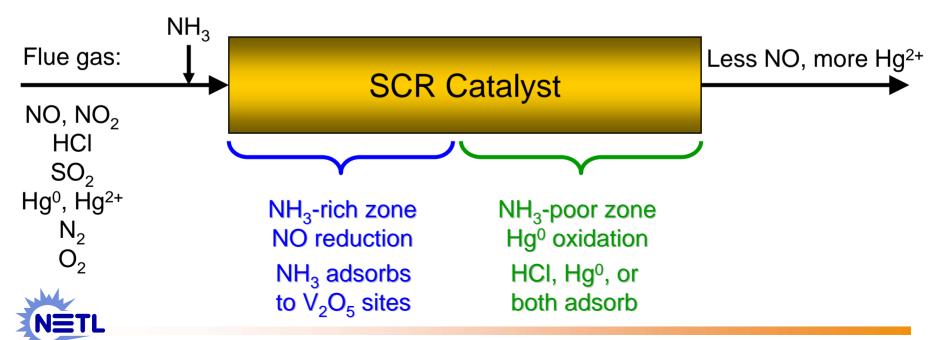
- Is Hg<sup>0</sup> physically or chemically adsorbed to sorbent surfaces?
- What are the intermediate products, if any?
- Is the final oxidized species HgCl<sub>2</sub>?
- What are the effects of co-reactants such as SO<sub>2</sub> and NO<sub>x</sub>?

Big picture: We lack predictive ability!



## **SCR Catalysts**

- Used for reduction of NO to N<sub>2</sub>
  - $-V_2O_5/WO_3$  on  $TiO_2$  support
  - $-T > 300^{\circ} C$



# **SCR Catalysts: Reaction**

#### Mechanism could be:

- Langmuir-Hinshelwood
- Eley-Rideal
  - Either HCl or Hg<sup>0</sup> adsorbed to surface

#### Likely competitive adsorption between NH<sub>3</sub> and HCl and/or Hg<sup>0</sup>

- Size of NH<sub>3</sub>-rich and NH<sub>3</sub>-poor zones determined by NH<sub>3</sub>/NO ratio
- Increasing NH<sub>3</sub>/NO reduces the extent of Hg<sup>0</sup> oxidation, and may force Hg<sup>0</sup> from the surface



# **SCR Catalysts: Results**

#### Laboratory scale

- ->95% oxidation of Hg<sup>0</sup> in simulated flue gas
- Slipstream of subbituminous/bituminous flue gas
  - 60-80% oxidation over 6 days
- Pilot scale test (bituminous coal)
  - SCR was placed downstream of ESP (T ~ 150° C)
  - Efficiency fell from 70% to 30% during 10-month test
  - Ash plugging may have been a problem

#### Full scale test

- Essentially no oxidation for lignite flue gas
- Ash plugged/blocked catalyst and limited both NO and Hg<sup>0</sup> conversion



# **SCR Catalysts: Outlook**

- Installing SCR for NO<sub>x</sub> reduction may provide co-benefit Hg<sup>0</sup> oxidation
  - Greatest benefit for bituminous coals (high CI)
  - Long-term conversion is uncertain
- Installing SCR catalyst specifically for Hg<sup>0</sup> oxidation may not be economical
  - Other materials are cheaper and give higher conversion to Hg<sup>2+</sup>



# **Carbon-based Catalysts**

- Carbon catalysts, activated carbons, fly ash, or Thief<sup>TM</sup> carbon
- Mercury adsorbs to carbon sites on fly ash particles
  - Hg(ads) is oxidized (chemisorbed) on carbon surfaces
  - Correlation between extent of oxidation and UBC in ash
  - Increased oxidation across baghouses



# **Carbon-based Catalysts: Reaction**

- HCl adsorbs to carbon sorbents
  - Langmuir-Hinshelwood mechanism
    - Adsorbed Hg<sup>0</sup> and HCl
  - Eley-Rideal mechanism
    - Either HCl or Hg<sup>0</sup> as adsorbed species
- NO appears to inhibit oxidation
- Role of SO<sub>2</sub> is unclear
  - -SO<sub>2</sub> can oxidize to H<sub>2</sub>SO<sub>4</sub> on activated carbon



# **Carbon-based Catalysts: Results**

- Carbon catalyst maintained >80% oxidation (pilot-scale) for two months
  - Effectiveness reduced by extended exposure to fly ash

#### Fly ash

Performance depends on source – high (>50%)
 conversion for bituminous ash, very low (<10%) for unpromoted lignite ash</li>

#### Thief carbon

- Achieved >70% oxidation in short-term tests
- No long-term tests



# **Carbon-based Catalysts: Outlook**

- Fly ash and Thief carbon may be economical
  - Inexpensive
  - Can be promoted with halogens
  - Regenerable
- Commercial carbon catalysts have shown good performance in pilot-scale tests
- These materials may be more cost-effective than metal or metal oxide catalysts



# **Metal and Metal Oxide Catalysts**

- Iron/Iron oxides
- Noble metals Cu, Pd, Au, Ag
- Ir and Ir/Pt
- $MnO_2$



# **Metal catalysts: Iron**

- Fe and Fe/Cr catalysts showed poor conversion
  - Studies suggest that stainless steel may catalyze oxidation
- Fe<sub>2</sub>O<sub>3</sub> may enhance Hg<sup>0</sup> oxidation on fly ash particles
  - Fe<sub>2</sub>O<sub>3</sub> in model fly ash (fixed bed) catalyzed oxidation
  - $-\alpha$  Fe<sub>2</sub>O<sub>3</sub> injected into flue gas had little catalytic ability
  - -γ- Fe<sub>2</sub>O<sub>3</sub> coated onto fabric filters enhanced oxidation
  - Catalytic effect of Fe<sub>2</sub>O<sub>3</sub> in fly ash may result from mix of species



## **Metal Catalysts: Noble Metals**

#### Palladium

- Most exhaustively tested noble metal catalyst
- Pilot-scale test using Pd deposited onto commercial forms
- ->80% oxidation for ten months
  - Sonic horns required to remove ash particles
- Preliminary economics
  - 62% savings over ACI for 80% Hg removal
  - 9% savings over ACI for 90% Hg removal



## **Metal Catalysts: Noble Metals**

#### Expect similar performance for Cu, Au, Ag as Pd

- Lack of mechanistic understanding is a hindrance!
- Example: Au catalyst
  - Meischen and Van Pelt: Hg<sup>0</sup> + HCl
  - Zhao et al: Hg<sup>0</sup> + Cl<sub>2</sub>; HCl reduced oxidation relative to Cl<sub>2</sub> alone

#### Cu is an interesting case

- CuO in a model fly ash oxidized >90% of Hg<sup>0</sup> from simulated flue gas
- CuCl can catalyze Hg<sup>0</sup> even without HCl (Mars-Maessen reaction?)



# **Metal Catalysts: Outlook**

- Noble metals (Pd) have promise
  - Possibly more cost-effective than ACI/COHPAC
  - Catalyst loading as little as 1 wt.%
- More work is required to better understand reaction dynamics



#### **Recommendations for Future Research**

- Understanding reaction mechanism and kinetics is paramount!
  - Predictive ability
  - Requires lab-scale tests using simulated flue gas
    - Downside: Differences between simulated and real flue gas
- Novel catalysts and catalyst supports
  - Cost effectiveness, regeneration

#### **Acknowledgments**

ORISE, IEP Program

